

IMPROVEMENTS IN METAL SALTS

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The present invention concerns improvements in metal salts, more especially concerns the removal of certain ions from aqueous solutions.

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It is commonplace in drilling for oil and gas, to use fluids such as brines as well servicing fluids. In general, such fluids have desirably a high density. In particular, highly concentrated alkali metal salts of carboxylic acids have been developed for use in oil and gas well drilling and completion operations. Such a fluid may be based upon cesium and potassium salts such as formates, which can provide brines of specific gravity values of 1.6 to 2.3, depending upon solution concentrations.

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During use of such brines, they may be contaminated with sodium chloride from sea water or from water or salt entrained within the rock and mud during application in the well bore. Chloride ions can cause severe corrosion of steel pipework and additionally may be incompatible with the rock matrix, causing damage to or near the well bore area. Such problems may result in users of such brines refusing to re-use chloride-contaminated brines. A charge of cesium formate solution for use as an oil field brine may cost in the order of \$10M, so there is considerable need to improve the prospects for recycling such a brine.

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Further, if a diluted brine is returned to high density by evaporation of water, any chloride concentration will increase by this process, thereby rendering the brine less suitable for re-use.

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Accordingly, the present invention can be applied to removal of chloride from brine both caused by contamination in use or caused by a concentration process such as evaporation, and throughout this description and claims the term "brine" is to be understood as including brines which have been concentrated.

The present invention provides a method of treating an alkali metal carboxylate salt brine contaminated with chloride ion, comprising mixing such contaminated brine with a

solution of a silver salt, especially silver nitrate, causing silver chloride to be formed and separating the silver chloride from the residual brine.

The invention may also be expressed as a method of use of an alkali metal  
5 carboxylate salt brine, comprising the recovery of used brine contaminated with chloride  
ion, treating the recovered brine with a solution of a silver salt, especially silver nitrate,  
causing silver chloride to be formed and separating the silver chloride from the brine, and  
re-using the brine. Desirably, the brine comprises cesium as the majority alkali metal by  
weight, and formate, acetate or other species, as the salt anion. The brine may comprise a  
10 significant proportion of other alkali metals, and may therefore contain mixtures of alkali  
metal carboxylates. Further, the brine may comprise one or more polymers or other  
components which are adjuvants and provide desirable properties to the brine or avoid  
disadvantages.

15 The preferred silver salt is silver nitrate, and for ease of description, all references  
hereinafter will be to silver nitrate.

Since the specific gravity of the brine is extremely important, it is desirable to  
minimise any loss of specific gravity by undue dilution during the treatment. Accordingly,  
20 it is desirable to use silver nitrate solutions containing at least 200g/l of  $\text{AgNO}_3$ , more  
preferably at least 300g/l  $\text{AgNO}_3$  and most preferably at least about 800g/l. At room  
temperature, saturation concentrations are about 1400g/l  $\text{AgNO}_3$ . The silver nitrate solution  
may contain other components which do not significantly adversely interfere with the  
method of the invention, or the performance of the brine. The silver nitrate solution is  
25 conveniently a product stream from a process involving the manufacture of high purity  
silver nitrate. This can provide economies arising from heat and water savings and other  
processing costs.

The treatment of the invention is conveniently carried out at room temperature, but  
30 may be carried out at higher or lower temperatures. It will be borne in mind that solubility  
decreases with decreasing temperature, and crystallisation may occur. Depending upon the

chloride concentration, it may be necessary to cool the brine to about 0°C, to facilitate the removal of sufficient nitrate salts formed as a by-product to create a stable solution that can be supplied and used in winter conditions.

5           Conveniently, silver chloride may be removed from the brine by filtration. This is particularly applicable because of the relatively high value of the silver chloride. Other methods for separation may be used, however, such as hydrocyclones or centrifuges, and where applicable or desirable, polymeric materials may be added to enhance separation.

10           The treatment may be carried out in a two-step process, or, in a preferred embodiment, in a single step process. Desirably, at least a 90% stoichiometric quantity of silver nitrate is used, relative to chloride ion, in the treatment. More desirably, the quantity of silver nitrate is from approximately 95% to approximately 112% stoichiometric, for brines containing 8.47 to 13.5g/l chloride. If the brine has other chloride contents or  
15           components, the stoichiometric adjustment may differ, which can be established by trial and error.

          The recovered silver chloride may carry entrained by-products such as silver formate and cesium nitrate. Under preferred conditions, these are minimised and removed to permit the production of a re-usable brine. By washing and crystallisation, silver chloride crystals  
20           may be obtained and the silver value recovered in conventional ways by conversion to other compounds or silver metal, using methods available to the person of ordinary skill in the art. In general, therefore, it is preferred to separate the silver chloride by filtration, but conventional washing of the solids is not desirable if it causes undue dilution of the filtrate. Entrained cesium formate in the filtered precipitate may be washed out subsequently, using  
25           water, and cesium nitrate may also be recovered if desired.

          The skilled person may use the information herein to optimise the process, using conventional techniques.

30           The invention may be further understood with reference to the following Examples.

**EXAMPLE 1****Stoichiometric Additions of AgNO<sub>3</sub>**

200 ml samples of a used cesium formate brine, containing 1587g/l cesium formate,  
 5 13.53g/l chloride, 0.720wt% sodium and 2.63 wt% potassium were used for all tests  
 described. Desirably, the chloride level will be reduced below 1g/l, more preferably  
 0.3 - 0.7g/l.

In the first Example, stoichiometric amounts of AgNO<sub>3</sub> solution are added with  
 10 stirring, to the brine, at room temperature and at differing concentrations:

AgNO <sub>3</sub> concn. (g/l)	150	200	600	918	1366
Volume added (ml)	87.6	65.7	21.6	14.5	9.5
Cl <sup>-</sup> concn. (g/l)	0.50	0.64	0.72-0.99	1.0	1.78
15 (all concentrations in g/l normalised to 200 ml)					
Specific gravity	1.848	1.913	2.084	2.117	2.129

In order to produce a product brine having Cl<sup>-</sup> concentration of approximately 0.5g/l,  
 combined with a specific gravity of not less than 2.0, a second stage treatment with AgNO<sub>3</sub>  
 20 was undertaken, with the following results:

First stage product Cl <sup>-</sup> (g/l normalised)	0.99	1.00	1.78
AgNO <sub>3</sub> stoichiometry (%)	50	50	80
AgNO <sub>3</sub> concn. (g/l normalised)	200	90	200
25 Final Cl <sup>-</sup> concn. (g/l normalised)	0.54	0.51	0.44
Overall AgNO <sub>3</sub> stoichiometry (%)	103.2	103.4	110.0
Specific gravity	2.055	2.077	2.057

After first and second stages, the deposits formed in the brine were filtered off.

**EXAMPLE 2****Single Stage Chloride Removal**

The identical cesium formate brine as in Example 1 was used in further tests, using  
5 differing stoichiometries:

Test No.	1	2	3
AgNO <sub>3</sub> stoichiometry (%)	107	110	116
10 Vol. AgNO <sub>3</sub> soln. added (ml)	10.2	10.4	11
Cl <sup>-</sup> concn. (g/l normalised)	0.58	0.35	<0.01
Specific gravity	2.111	2.122	2.095

Tests 1 and 2 proceeded satisfactorily at room temperature. It was assessed in Test 3 that  
15 excess silver was being dissolved and a post-treatment of heating the product brine to 95°C was incorporated, to remove the silver in solution.

A further post treatment of cooling to approximately 0°C overnight followed by  
filtration, was found to remove a large proportion of by-product cesium nitrate, leaving a stable  
20 clear solution at room temperature.

**EXAMPLE 3****Single Stage Chloride Removal from a K/Cs Formate Brine**

25 200ml samples of a potassium/cesium formate brine, containing 497g/l formate and 8.47g/l chloride, 0.675wt%sodium, 12.56wt% potassium and 33.9wt% cesium were used for all the tests described in this Example 3. Desirably, the chloride level will be reduced such that it lies in the range 0.7 to 1.0g/l.

30 An orthogonal array of sixteen tests in which different concentrations and stoichiometric amounts of AgNO<sub>3</sub> are added at different temperatures, with different stirring

rates, addition rates and residence times is shown below. In the tests in this Example, the reactants were stirred with an IKA Werke RCT-Basic stirrer, using either a "Slow" setting (setting 4) or a "Fast" setting (setting 7). Addition rate was either "Slow" or "Fast", corresponding to a 15 minute addition time or a 30 second addition time, respectively.

- 5 Residence times are the times from addition of the last drop of  $\text{AgNO}_3$  to the beginning of filtration, and "Short" means 5 minutes and "Long" means 30 minutes.

$\text{AgNO}_3$ conc. (g/l)	Stoichio- metry (%)	Temp- erature (°C)	Stir Rate	Addition Rate	Residence Time	Norm. $\text{Cl}^-$ conc. (g/l)	Specific Gravity
600	95	25	Fast	Fast	Short	0.68	1.859
600	100	25	Slow	Fast	Long	0.81	1.867
600	105	35	Fast	Slow	Long	0.01	1.847
600	110	35	Slow	Slow	Short	0.38	1.848
800	95	35	Slow	Fast	Long	1.61	1.867
800	100	35	Fast	Fast	Short	0.42	1.871
800	105	25	Slow	Slow	Short	0.71	1.856
800	110	25	Fast	Slow	Long	0.01	1.851
1000	95	25	Slow	Slow	Long	1.86	1.856
1000	100	25	Fast	Slow	Short	0.41	1.857
1000	105	35	Slow	Fast	Short	1.37	1.871
1000	110	35	Fast	Fast	Long	0.01	1.868
1200	95	35	Fast	Slow	Short	0.87	1.884
1200	100	35	Slow	Slow	Long	1.84	1.886
1200	105	25	Fast	Fast	Long	0.14	1.871
1200	110	25	Slow	Fast	Short	3.26	1.865

- 10 By following the orthogonal matrix, it can be demonstrated that the chloride level can be reduced from 8.47g/l to between 3.26 and <0.01g/l by the addition of  $\text{AgNO}_3$  under various conditions.

Analysis of the chloride levels observed by following the orthogonal matrix suggests that the stirring rate, concentration and stoichiometry of the  $\text{AgNO}_3$  added, are the most significant factors that determine the post-treatment chloride level in descending order of importance. In particular, a fast stirring rate is highly desirable for efficient  $\text{AgCl}$  precipitation as the formate reduction of silver side reaction is minimised. The temperature, addition rate and residence time appear to be less significant factors.

To validate the conclusions drawn from the orthogonal array, a further three confirmation tests were designed specifically to reduce the post-treatment chloride level to 0.85, 0.65 and 0.45g/l. The same brine was treated at 35°C, with the  $\text{AgNO}_3$  added slowly with fast stirring before a long residence time.

Test No.	1	2	3
AgNO <sub>3</sub> stoichiometry (%)	95	95	100
AgNO <sub>3</sub> concentration (g/l)	1200	800	1000
Target Cl <sup>-</sup> level	0.85	0.65	0.45
Cl <sup>-</sup> concentration (normalised, g/l)	0.88	0.66	0.37
SG	1.890	1.874	1.884

The most  $\text{AgNO}_3$  efficient reduction in Cl<sup>-</sup> level from 8.47 to <1g/l and the lowest amount of water added occurs in Test 1.